



Acid catalyzed alkylation of phenols with cyclohexene: Comparison between homogeneous and heterogeneous catalysis, influence of cyclohexyl phenyl ether equilibrium and of the substituent on reaction rate and selectivity

L. Ronchin*, A. Vavasori, L. Toniolo

Department of Molecular Science and Nanosystems, University Ca' Foscari of Venice, Dorsoduro 2137, 30123 Venice, Italy

ARTICLE INFO

Article history:

Received 1 August 2011
Received in revised form
28 November 2011
Accepted 7 December 2011
Available online 16 December 2011

Keywords:

Acid catalysis
Sulfonated resins
Phenols alkylation
Alkylation selectivity

ABSTRACT

The reactivity of several phenols toward liquid phase alkylation with cyclohexene in the presence of heterogeneous and homogeneous acid catalyst at 358 K is studied. The comparison between Amberlyst 15 and $\text{CH}_3\text{SO}_3\text{H}$, as examples of heterogeneous and homogeneous systems, shows a higher activity of the former with different behavior of selectivity between the two systems, anyway, in both systems O-alkylation and ring alkylations occur. A remarkable difference in the selectivity of the ring alkylation between heterogeneous and homogeneous systems is observed: Amberlyst 15 shows a constant *ortho/para* ratio close to 2, while in the presence of $\text{CH}_3\text{SO}_3\text{H}$ *ortho/para* is variable from 3 to 5, suggesting an involvement of the cyclohexyl phenyl ether rearrangement. This is proved also by a direct relationship between the *ortho/para* ratio and the concentration of the cyclohexyl phenyl ether when $\text{CH}_3\text{SO}_3\text{H}$ is used as a catalyst. The formation of cyclohexyl aryl ethers is reversible; on the contrary, ring alkylation appears irreversible. The reactivity of the dimethylphenols shows a strong influence of the steric hindrance of the substituent on the electrophilic attack of the cyclohexyl cation, which is poorly influenced by the inductive effect of the methyl group.

© 2011 Published by Elsevier B.V.

1. Introduction

Organic industrial processes employ acid catalyzed reactions such as alkylation, acylation, isomerization, cracking, nitration, condensation, esterification, etc. The green technologies in order to replace the traditional polluting mineral acid catalysts with solid ones are continuously improved [1–6]. Zeolites, acid treated clays, ion exchange resins and supported acids are investigated by several researchers for their application in pharmaceutical, perfumery, agro-chemicals, dye-stuffs, intermediates and specialty chemical industries [5–12]. Alkylation reactions in particular are really important in the industrial synthesis of many large scale production compounds [11,12].

Alkylation of phenol with cyclohexene has attracted considerable interest because of its industrial and academic relevance [13–21]. This reaction leads to a variety of products such as 4-cyclohexylphenol, 2-cyclohexylphenol, and cyclohexyl phenyl ether depending on both the catalyst and the reaction conditions. The use of solid acid catalysts appears a suitable alternative to the usual procedures in homogeneous phase with catalysts such as AlCl_3 , BF_3 , TiCl_4 , HF. On considering the current effort toward

process innovation aimed to avoid environmental concerns, ion-exchange resins appear to be ideal catalysts to convert polluting processes into greener ones [2–6].

In a large number of industrial processes the cation-exchange resins are used as a catalyst such as in MTBE or TAME synthesis, the manufacture of alkyl phenols and bisphenol A, the esterification of a variety of carboxylic acids, the hydration of alkenes, the dimerization of isobutene, etc. [4–6,19,22,23].

The mechanism of acid catalyzed alkylation is well known for a long time and it is widely accepted the carbonium ion attack to the electronic rich center as the key step of the reaction [24,25]. Cyclohexene in the presence of acid gives the cyclohexyl cation as a transient species that readily reacts with a nucleophile giving the corresponding cyclohexyl derivative. The rearrangement to the more stable methyl cyclopentyl cation occurs only in a negligible extent since the skeleton rearrangement is slower than the nucleophilic attack, which occurs, for many nucleophiles, at encounter [26].

The study of Richard and coworkers on the reactivity of phenol as nucleophile toward methyl phenyl carbocation showed that the relative rates for alkylation of phenol at $-\text{OH}$, C-4 and C-2 are 230:20:1, respectively. On the contrary, the alkylation of the corresponding nucleophilic sites of phenoxide ion, which is an encounter reaction, showed the relative rates of 2:2:1 [27]. Other authors pointed out that the selectivity toward the *ortho* position in the

* Corresponding author. Fax: +39 0412348517.
E-mail address: ronchin@unive.it (L. Ronchin).

phenol alkylation is favored when the less hindered secondary carbonium ions are the electrophiles, while tertiary carbocations give prevalently *para* alkylation [28,29]. The studies of Sharma and coworkers, carried out in the early ninety relating the reactivity of phenol in the presence of sulfonated resins, pointed out that the *ortho-para* selectivity in the ring alkylation of phenol is strictly related to the nature of the olefin employed. In particular, propene and 1-butene give an *ortho-para* ratio close to 2, while isobutene, α -methyl styrene and diisobutene give almost exclusively *para* alkylation [29]. Recently, Bhatt and Patel reported that supported 12-tungstosilicic acid catalyzes only ring cyclohexylation of phenol giving an *ortho-para* ratio close to 2 [15]. More recently, Hölderich and coworkers showed that high *para* selectivity is obtained in the alkylation of phenol with isobutene in the presence of catalysts with Lewis or Brønsted acid sites, indifferently. The selectivity is not sensible to the type of acid present in the catalyst but the activity is influenced by the amount and the strength of the sites [30].

The comparison of activity and selectivity between heterogeneous and homogeneous BF_3/SiO_2 and $\text{BF}_3 \cdot (\text{H}_2\text{O})_2$ catalysts was studied by Clark and coworkers [21]. They pointed out that cyclohexyl phenyl ether, and cyclohexyl phenols are formed in the presence of both systems, but only by the homogeneous $\text{BF}_3 \cdot (\text{H}_2\text{O})_2$ as a catalyst the rearrangement of the ether to alkyl phenols is observed [21]. Yadav and Kumar have recently studied the kinetics of phenol cyclohexylation catalyzed by different solid acids, which catalyze the formation of phenyl cyclohexyl ether and the products of ring alkylation in a *ortho-para* ratio close to 2 [14]. The mechanistic aspect of the electrophilic attack to the phenol is investigated from a theoretical point of view by Tang and coworkers. These authors suggested that the addition of the sulfonic acid to the olefins occurs leading to the formation of a sulfonic ester intermediate, which, in turns, reacts with phenol to form the products of alkylation [31].

In this paper we study the cyclohexylation of some phenols and the reactivity of cyclohexyl phenyl ether in the presence of both $\text{CH}_3\text{SO}_3\text{H}$ and sulfonic resins. In particular, we investigate the role of the cyclohexyl phenyl ether on the *ortho-para* selectivity and the reactivity of the dimethylphenols in order to account for the steric hindrance of the methyl groups on the electrophilic attack of the cyclohexyl cation.

2. Experimental

2.1. Materials

Reagents and solvents were used after purification of the commercially available samples and their purity was checked by the usual methods (melting point, TLC, HPLC, GC and GC-MS). The solvents were treated in a double bed column, filled with $\text{H}_2\text{SO}_4/\text{SiO}_2$ and SiO_2 to adsorb water and impurities. The residual water content was checked by HPLC analysis [32]. Commercial catalysts: macroreticular sulfonated styrene divinyl benzene resins Amberlyst 15TM and Amberlyst 36TM (a trade mark of Rohm and Haas) were purchased from Aldrich.

2.2. Reactions

The reactions and the kinetic runs were performed in a stirred glass reactor thermostatted by a circulation bath at 358 K, containing weighed samples of solvent, reagents and catalyst at autogenous solvent pressure (122 and 158 kPa for 1,2 dichloroethane and benzene, respectively). In a typical experiment 10 mL of solution containing 10 mmol of phenol, 10 mmol of cyclohexene plus 5 mmol of methylcyclohexane as internal standard and the desired amount of catalyst (100–500 mg) were placed in the

reactor. All the operations were carried out into a glove box in order to minimize catalyst deactivation by air moisture. Small amounts of the solution were drawn at different times and the samples were analyzed by GC, and GC-MS using a HP5 capillary column (300 μm i.d. 30 m long, 95% methyl, 5% phenyl silicone phase). The samples were checked also by HPLC using a Perkin Elmer apparatus and a Lichrosphere 100 (RP-18, 5 μm) column. The first derivative at time 0 of a third order polynomial function, obtained by fitting cyclohexene concentration vs. time at 10% of conversion, gave the initial rate of reaction.

For a reliable comparison of the performances of different catalysts it is essential to know if reaction rate data are affected by diffusion phenomena. This is verified by studying the influence of the granulometry and of the catalyst amount on the reaction rate catalyzed by the most active catalyst (Amberlyst 36) at 373 K. The experimental evidences suggest that the kinetics is not influenced by diffusion phenomena, since there are no differences in the initial rate using resins with different granulometry and the initial reaction rates are strictly proportional to the catalyst amount. In addition, the inspection of Carberry and Wheeler-Weisz numbers shows values lower than 0.1 and 0.4, respectively [33].

3. Results and discussion

3.1. Influence of solvent and catalyst on reaction rate, conversion and selectivity

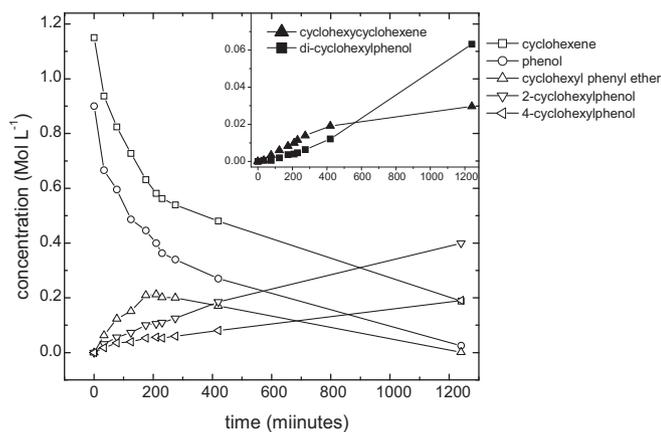
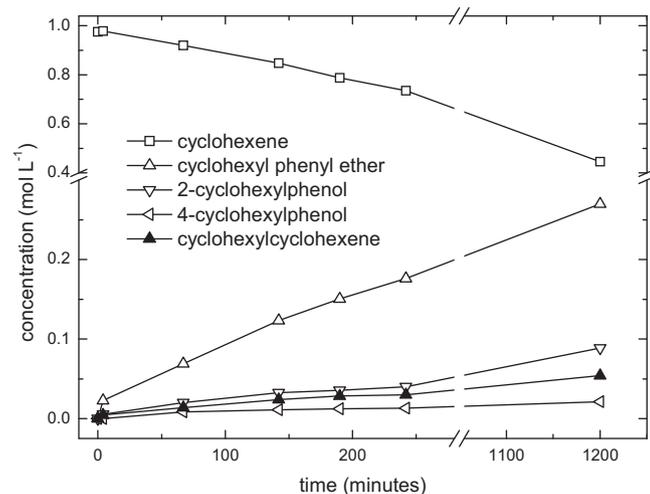
Table 1 reports the activity of two sulfonated resins in the alkylation of phenol. Maximum yield, as reported in Table 1, is comprised between 20 and 26% at 40–50% of conversion. Despite of Amberlyst 36 promotes a initial rate of reaction higher than that of Amberlyst 15, the latter gives the highest yield in the ether. As a matter of fact, Amberlyst 36 (5.5 meq. $\text{H}^+ \text{g}^{-1}_{\text{cat}}$) shows a higher activity than the Amberlyst 15 (4.7 meq. $\text{H}^+ \text{g}^{-1}_{\text{cat}}$), this is likely due to the higher acid content of the former. In fact, the activities of the two catalysts are quite similar considering the initial turnover frequency referred to the whole H^+ sites (Table 1). $\text{CH}_3\text{SO}_3\text{H}$ (in homogeneous phase) is the least active catalyst and its TOF is 20 times lower than that of the sulfonic resins, likely due to the higher acidity of the latter [34]. As a matter of fact, by considering *p*-toluenesulfonic acid as simplified model for the sulfonic resins, the $\text{p}K_a$ of the *p*-toluenesulfonic acids is 2.7 $\text{p}K_a$ units lower than that of methanesulfonic acid (–4.7 and –2, respectively) [35]. In the presence of AlCl_3 the reaction is faster, but the comparison of the activities of sulfonated resins, methanesulfonic acid (protic acids) and AlCl_3 (Lewis acid) is cumbersome due to the different nature of the acid site. It is noticeable that the reactivity of the *ortho* and *para* positions of phenol is not influenced by the type of sulfonic resins employed. *Ortho*- and *para*-positions of the phenol show similar relative reactivity giving *ortho-para* ratio $\cong 2$ in either benzene or 1,2-dichloroethane. In contrast, a not negligible solvent effect seems to be played by nitromethane, since the initial reaction rates are almost one order of magnitude lower than those measured in benzene and 1,2-dichloroethane. In addition, the *ortho-para* ratio clearly diminishes (*o/p* $\cong 1.5$), thus suggesting an influence of the solvent on the electrophilic attack [36].

Despite of the large difference of activity between $\text{CH}_3\text{SO}_3\text{H}$ and AlCl_3 in homogeneous phase, the reactions show a similar *o/p* ratio (4.2 and 4.5), thus suggesting similar relative reaction rate for each stage in this homogeneous reactions.

The concentration–time profiles reported in Figs. 1–3, relative to the reactions in the presence of Amberlyst 15, $\text{CH}_3\text{SO}_3\text{H}$ and AlCl_3 , respectively, show different trends. Fig. 1 reports the reaction catalyzed by Amberlyst 15. It appears that cyclohexyl phenyl ether is a transient species, which is almost completely consumed at the end of the reaction. On the contrary, the formation of cyclohexyl,

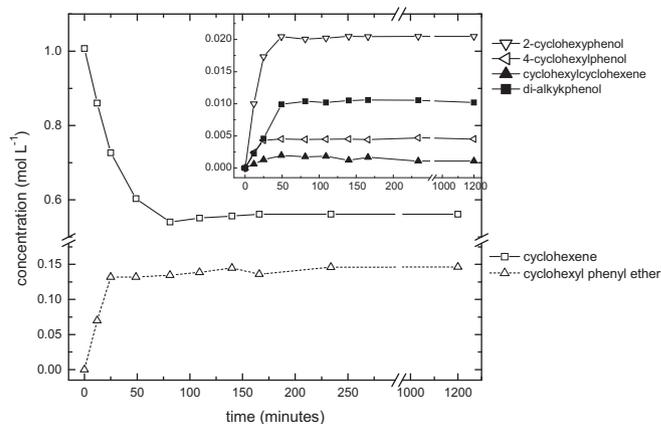
Table 1Alkylation of phenol: selectivity after 240 min of reaction at 358 K. Run conditions: phenol 1.1 mol L⁻¹, cyclohexene 1.1 mol L⁻¹, catalyst 400 mg, reaction volume 10 mL.

Catalyst	Conv. (%)	r_0^a	TOF ^b	Ether maximum yield (%)	Selectivity ^c (%)				o/p
					2-Cyclohexyl phenol	4-Cyclohexyl phenol	Dicyclohexyl phenols	Cyclohexyl cyclohexene	
Benzene									
Amb.15	42	15	5.3	25	29	16	13	15	1.9
Amb. 36	48	18	5.8	23	38	21	14	18	1.9
1,2-Dichloroethane									
Amb.15	51	18	6.8	26	29	14	15	12	2.0
Amb.36	64	22	6.9	23	31	16	18	15	1.9
CH ₃ SO ₃ H ^d	21	3.5	0.34	17	10	2.4	2.3	2	4.2
AlCl ₃ ^{d,e}	44	58	7.7	15	5	1.1	4.6	1	4.5
Nitromethane									
Amb.15	16	3.8	0.81	10	24	16	Traces	Traces	1.5
Amb.36	19	6.0	1.1	10	24	16	Traces	Traces	1.5

^a (10⁵ mol L⁻¹ s⁻¹ g_{cat}⁻¹).^b Initial turnover frequency (10⁴ s⁻¹).^c Products in trace amount, as the isomers of alkylated the cyclohexyl ether, has been neglected.^d Homogeneous reactions.^e T 288 K, AlCl₃ 1 mmol.**Fig. 1.** Reaction profile of alkylation of phenol at 358 K catalyzed by Amberlyst 36. Run conditions: phenol 1.1 mol L⁻¹, cyclohexene 1.2 mol L⁻¹, catalyst 400 mg, solvent 1,2-dichloroethane, reaction volume 10 mL.**Fig. 2.** Reaction profile of alkylation of phenol at 358 K catalyzed by methanesulfonic acid. Run conditions: phenol 1 mol L⁻¹, cyclohexene 1 mol L⁻¹, catalyst 400 mg, solvent 1,2-dichloroethane, reaction volume 10 mL.

di-cyclohexyl phenols increases monotonically during the reaction course. Formation of di-cyclohexyl phenols is observed also at very low conversion, because of alkyl phenols are highly activated toward the electrophilic attack [37]. Under the conditions used the main side reaction is cyclohexene dimerization, whose product (cyclohexylcyclohexene) shows an almost linear monotonic increase during reaction course. It is noteworthy that dimer formation is strongly inhibited using nitromethane as the solvent, suggesting an inhibiting effect of the solvent on the formation of the electrophile [36].

Fig. 2 shows the reaction profile in the presence of CH₃SO₃H: the reaction is almost ten times slower than that in the presence of Amberlyst 15 as a catalyst (Table 1) and after 20 h of reaction all the products are still increasing, while the formation of di-cyclohexyl phenols is negligible. The concentration–time profile of phenol cyclohexylation catalyzed by AlCl₃ (Fig. 3) evidences a fast reaction also at 288 K (almost twice of that measured in the presence of Amberlyst 15 at 358 K) but the reaction completely stops after 55 min, with a modest conversion and with a noticeable loss of the mass balance. Such a behavior suggests a fast catalyst deactivation due to the formation of heavy pitch, which is confirmed by HPLC analysis.

**Fig. 3.** Reaction profile of alkylation of phenol catalyzed by AlCl₃ at 288 K. Run conditions: phenol 1 mol L⁻¹, cyclohexene 1 mol L⁻¹, catalyst 140 mg, solvent 1,2-dichloroethane, reaction volume 10 mL.

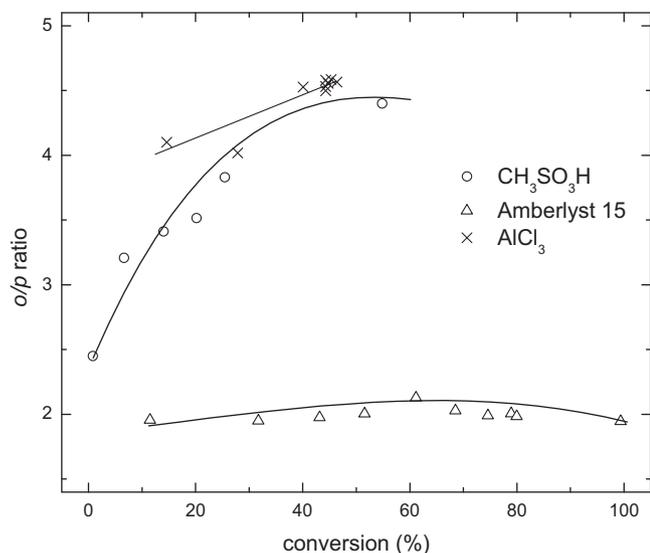


Fig. 4. Comparison of *ortho/para* ratio vs. conversion in the cyclohexylation of phenol in the presence of liquid and solid acid catalysts. Run conditions: cyclohexene and phenol 1 mol L^{-1} , Amberlyst 15 and $\text{CH}_3\text{SO}_3\text{H}$ 1.8 meq H^+ , AlCl_3 10 mmol , solvent 1,2-dichloroethane, reaction volume 10 mL T 358 K .

In Fig. 4 the trend of the *ortho*–*para* ratio vs. conversion for each catalyst is reported. Employing Amberlyst 15 as a catalyst *ortho*–*para* ratio remains practically constant (1.9–2.1), whereas, in the presence of $\text{CH}_3\text{SO}_3\text{H}$, monotonically increases from 2.4 to 4.2 as the conversion increases. Also in the presence of AlCl_3 , the *ortho*–*para* ratio vs. conversion increases from 4.1 to 4.5. These evidences suggest a different nature in the formation of the *ortho* and *para* isomers as the catalyst nature change. This is confirmed by the trends of the *ortho*–*para* ratio vs. cyclohexyl phenyl ether concentration reported in Fig. 5. Clearly, there is a linear relationship between the ether concentration and the formation of the *ortho* isomer in the presence of $\text{CH}_3\text{SO}_3\text{H}$, thus suggesting the involvement of the cyclohexyl phenyl ether in the formation of the *ortho* isomer, likely *via* rearrangement [37,38]. On the contrary, in the presence of Amberlyst 15, there is a very small influence of the concentration of

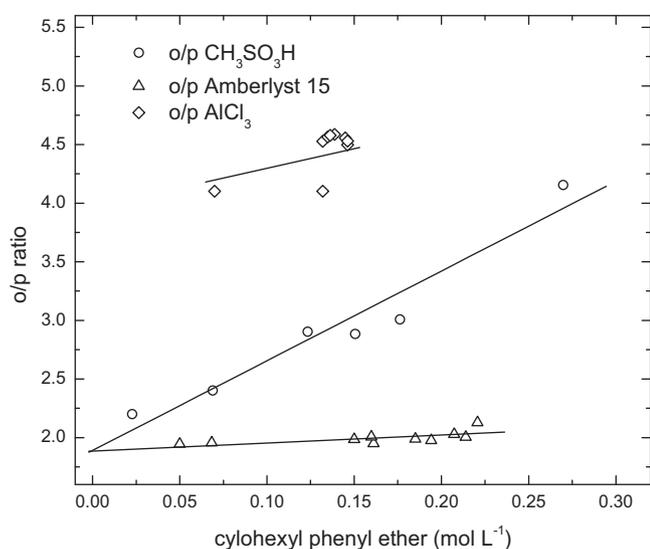


Fig. 5. Comparison of *ortho/para* ratio vs. cyclohexyl phenyl ether concentration in the cyclohexylation of phenol in the presence of liquid and solid acid catalysts. Run conditions: cyclohexene and phenol 1 mol L^{-1} , Amberlyst 15, 400 mg , $\text{CH}_3\text{SO}_3\text{H}$ 1.8 meq H^+ and AlCl_3 1 mmol , solvent 1,2-dichloroethane, reaction volume 10 mL T 358 K .

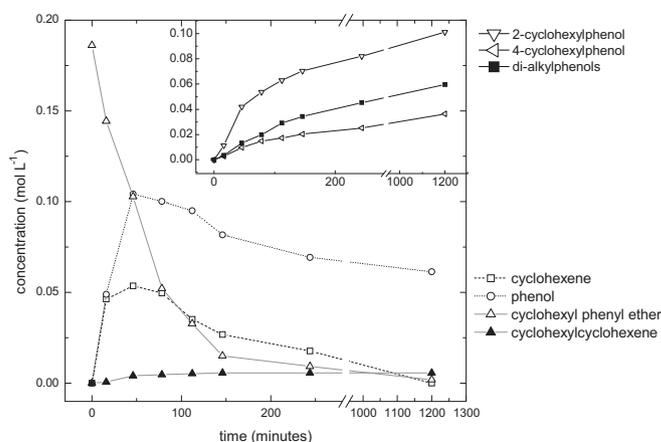


Fig. 6. Reactivity of cyclohexyl phenyl ether. Run conditions: T 358 K Amberlyst 15, 400 mg , solvent 1,2-dichloroethane, reaction volume 10 mL .

the cyclohexyl phenyl ether toward *ortho* and *para* selectivity. Such a behavior suggests that, in the presence of Amberlyst 15, the *ortho* and *para* selectivity is mainly influenced by the mesomeric effect of the hydroxyl group [37–39]. Besides the reaction catalyzed by AlCl_3 shows a small increase of the *ortho/para* ratio vs. cyclohexyl phenyl ether concentration, but with a neat prevalence of the *ortho* isomer. The reasons of such a behavior are not clear and at least two effects may concur to give this result: the ether rearrangement and a specific interaction between phenol and AlCl_3 , as suggested by Sartori and coworkers [40].

3.2. Reactivity of cyclohexyl phenyl ether

The reactivity of cyclohexyl phenyl ether, in presence of acid catalysts, is reported in Figs. 6–8 and in Table 2. Fig. 6 shows the concentration–time profile of the reaction catalyzed by Amberlyst 15: cyclohexene reaches a maximum after 2 h of reaction, and then it decreases to complete consumption. At the same time, phenol concentration reaches to a maximum and subsequently diminishes smoothly (almost to a plateau). As a matter of fact, phenol is less converted than cyclohexene because all reactions, such as alkylation, dialkylation and cyclohexene dimerization, concur to consume cyclohexene. The initial reaction rate of ether decomposition is comparable to that of the phenol cyclohexylation and

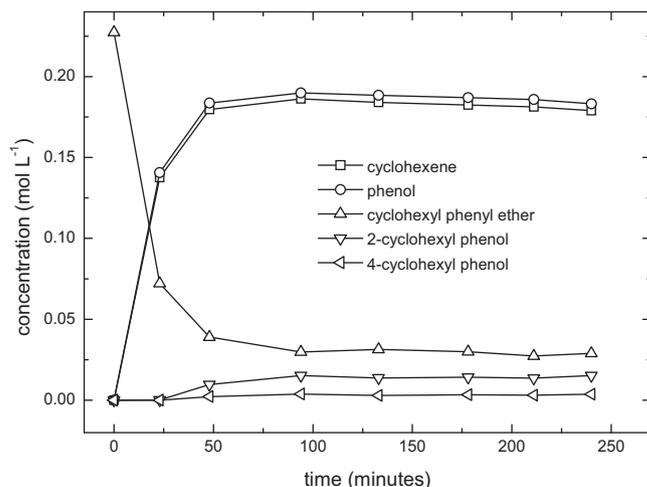


Fig. 7. Reactivity of cyclohexyl phenyl ether. Run conditions: cyclohexyl phenyl ether 0.21 mol L^{-1} , T 358 K , $\text{CH}_3\text{SO}_3\text{H}$ 180 mg , solvent 1,2-dichloroethane, reaction volume 10 mL .

Table 2
Reactivity of cyclohexyl phenyl ether: selectivity after 240 min of reaction at 358 K. Run conditions: cyclohexyl phenyl ether 0.2 mol L^{-1} , solvent 1,2-dichloroethane, reaction volume 10 mL.

Catalyst	Conv. (%)	r_0^a	Selectivity (%)			<i>o/p</i> Ratio
			2-Cyclohexyl phenol	4-Cyclohexyl Phenol	Dicyclohexyl phenols	
Amberlyst 15 ^b	92	10	10	33	18	3.3
$\text{CH}_3\text{SO}_3\text{H}^c$	85	40	4	0.9	Traces	4.2
AlCl_3^d	74	75	19	3.4	22	5.6

^a ($10^5 \text{ mol L}^{-1} \text{ s}^{-1} \text{ g}^{-1} \text{ cat}$).

^b Amberlyst 15, 400 mg.

^c $\text{CH}_3\text{SO}_3\text{H}$ 180 mg.

^d T 288 K, AlCl_3 0.2 mmol.

considering the whole reaction steps, ring alkylations are likely the slower stage, thus allowing accumulation of phenol and cyclohexene. In the presence of $\text{CH}_3\text{SO}_3\text{H}$ (Fig. 7) the reverse etherification occurs with an initial reaction rate 4 times higher than when Amberlyst 15 is used as a catalyst, and after 50 min of reaction 75% of cyclohexyl phenyl ether is converted to cyclohexene and phenol in 95% of overall selectivity. In fact, $\text{CH}_3\text{SO}_3\text{H}$ as a catalyst does not give ring alkylation products in high yields, but allows fast decomposition of the ether. Fig. 8 shows the concentration–time profile of the reactivity of the cyclohexyl phenyl ether at 288 K, in the presence of AlCl_3 , the initial reaction rate is much higher than in the presence of Amberlyst 15 (7 times) but it does not reach completeness probably because of catalyst poisoning, in agreement to what found in phenol alkylation. In this case, the concentration of cyclohexene is negligible with respect to that of phenol, due to a fast formation of cyclohexene oligomerization products, which are probably one of the reasons of catalyst deactivation.

The *ortho/para* selectivity (see Table 2) with different catalysts after 4 h of reaction is in the range 3.3–5.6, and, as expected, the ether favors the *ortho*-selectivity. Apparently, the trends of the *o/p* ratio vs. ether conversion, showed in Fig. 9, are not in agreement with those found in the phenol cyclohexylation (Fig. 5), because both AlCl_3 and $\text{CH}_3\text{SO}_3\text{H}$ show a constant *o/p* ratio (5.3, 4.3, respectively), while in the presence of Amberlyst 15 the *o/p* ratio decreases from 4.2 to 2.7. Despite of the complexity of the reaction it is clear that cyclohexyl phenyl ether is involved in the selectivity of the *ortho* and *para* isomers of the alkylated phenols, but further investigations needs to highlight such a behavior.

3.3. Reactivity of dimethylphenols and 2,4,6-trimethylphenol

Further insight on the reactivity of the cyclohexyl cation as electrophile toward phenols may be gained by studying the reactivity of dimethylphenols and of the 2,4,6-trimethylphenol, in order to test the influence of the methyl substituent both for its inductive effect as well as for the steric hindrance. In Figs. 10 and 11, the concentration–time profile of the cyclohexylation of the 2,3-dimethylphenol catalyzed by both Amberlyst 15 and $\text{CH}_3\text{SO}_3\text{H}$ are shown. The general trend observed in this case is similar for all phenols, thus suggesting the involvement of a same reaction path. In agreement with that observed for the phenol the activity of the Amberlyst 15 is, in any case, higher than that of $\text{CH}_3\text{SO}_3\text{H}$ (Table 3), which is likely due to the superior protonation ability of the solid acid with respect to the liquid one [34,35]. The activity of 3,5-dimethyl phenol and 2,6-dimethyl phenol are lower than that of neat phenol (Table 1), the phenomenon may be ascribed to the steric hindrance of the substituents, which slow down the electrophilic attack [37,38]. Such an effect is more pronounced on the initial reaction rate of the 2,6-isomer than the 3,5-one. The small increase of the reaction rate of the 2,3-dimethyl-phenol cyclohexylation with respect to that of neat phenol may be due to the inductive effect of methyl groups, even though the steric hindrance may play a non-negligible effect. In fact, the initial reaction rate of 2,4-dimethyl-phenol is equivalent to that of phenol, the reason of this behavior is not clear, but it might be ascribed to the

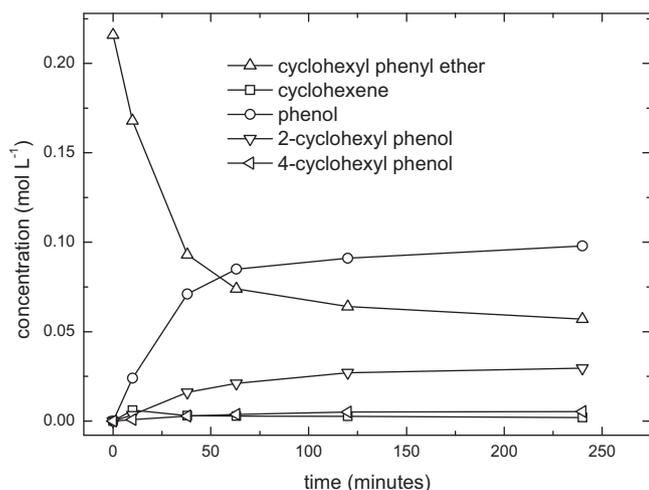


Fig. 8. Reactivity of cyclohexyl phenyl ether. Run conditions: cyclohexyl phenyl ether 0.21 mol L^{-1} , T 358 K, AlCl_3 1 mmol, solvent 1,2-dichloroethane, reaction volume 10 mL.

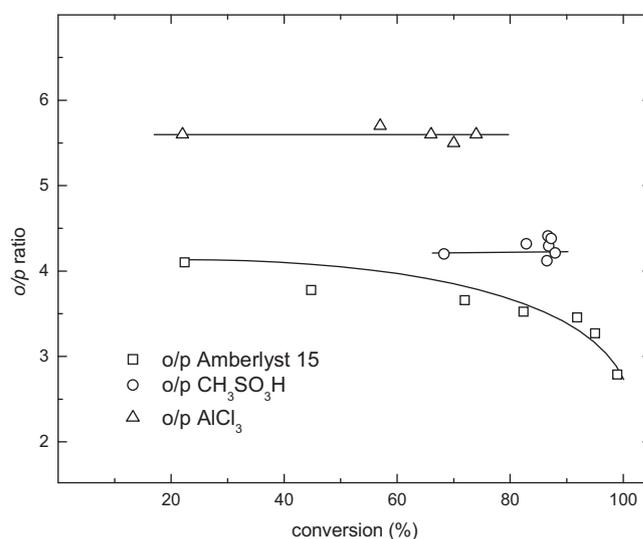


Fig. 9. Comparison of *ortho/para* ratio vs. conversion in the cyclohexylation of phenol and in the rearrangement of cyclohexyl phenyl ether. Run conditions: cyclohexene and phenol 1 mol L^{-1} , Amberlyst 15, $\text{CH}_3\text{SO}_3\text{H}$ 1.8 meq H^+ and AlCl_3 1 mmol as catalysts, solvent 1,2-dichloroethane, reaction volume 10 mL T 358 K. Cyclohexyl phenyl ether rearrangement are carried out with the same run conditions except the initial concentration of 0.2 mol L^{-1} .

Table 3

Alkylation of dimethylphenols and 2,4,6-trimethylphenol: selectivity after 240 min of reaction at 358 K. Run conditions: dimethylphenols 1.2 mol L⁻¹, cyclohexene 1.1 mol L⁻¹, Amberlyst 15, 400 mg or CH₃SO₃H 180 mg, solvent 1,2-dichloroethane, reaction volume 10 mL.

Catalyst	Conv. (%)	r_0^a	Selectivity (%)				
			Ether	2-Cyclohexyl DMP ^b	3-Cyclohexyl DMP ^b	4-Cyclohexyl DMP ^b	Cyclohexyl cyclohexene
2,6-Dimethylphenol							
Amberlyst 15	15	2.6	26	–	5	15	13
CH ₃ SO ₃ H	7.2	0.9	18	–	11	16	55
3,5-Dimethylphenol							
Amberlyst 15	35	16	24	27	–	5	10
CH ₃ SO ₃ H	14	4.1	29	14	–	0.1	13
2,3-Dimethylphenol							
Amberlyst 15	95	44	4	38	5	12	4
CH ₃ SO ₃ H	13	3.1	18	19	–	5	55
2,4-Dimethylphenol							
Amberlyst 15	80	30	10	42	10 ^c	–	5
CH ₃ SO ₃ H	12	2.1	12	10	2 ^c	–	62
2,5-Dimethylphenol							
Amberlyst 15	57	14	16	16	–	16	2
CH ₃ SO ₃ H	16	1.5	16	9	–	4	15
2,4,6-Trimethylphenol							
Amberlyst 15 ^c	1	0.2	–	–	–	–	50
CH ₃ SO ₃ H ^c	5	0.6	–	–	–	–	50

^a (10⁵ mol L⁻¹ s⁻¹ g_{cat}⁻¹).

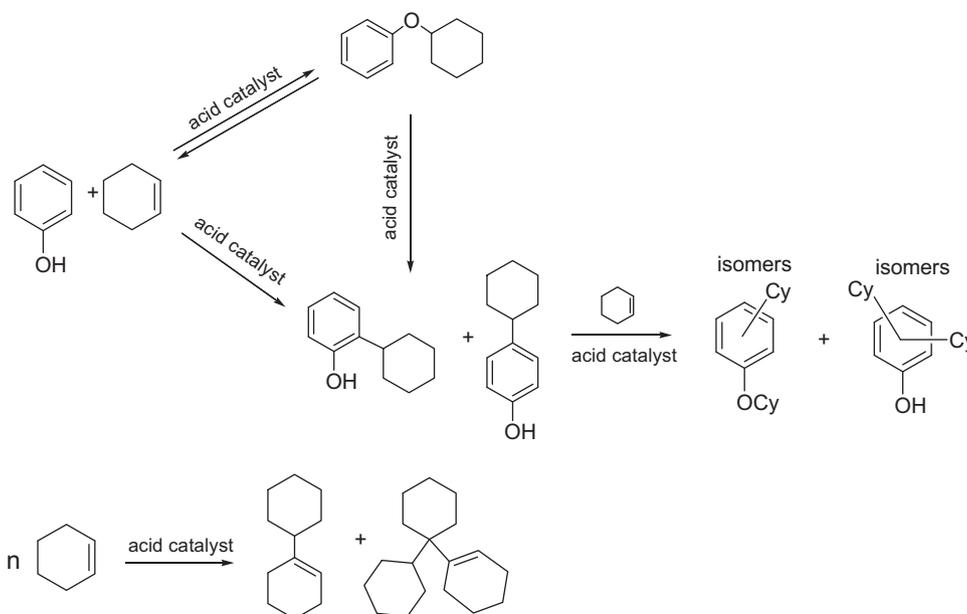
^b DMP = dimethylphenol.

^c Between the two possible isomer (in 3 or 5 position) it has not verified what is formed, but the 5 isomer is more plausible, due to the lower steric hindrance of the 5 position.

^d Large part of the products are peach, formation of traces of the ether and the m-isomer has been observed after 20 h of reaction.

simultaneous presence of two contrary effects: the steric hindrance and the inductive effect of the methyl groups. The reactivity of 2,5-dimethyl-phenol is clearly influenced by the steric hindrance of the methyl groups, in particular the one in 2-positions slows down the attack of the cyclohexyl cation toward the hydroxyl group, while that in 5-position simultaneously hampers the attack to both *ortho* and *para* positions. As a matter of fact, 2,4,6-trimethyl-phenol shows a negligible reactivity toward electrophilic attack, thus suggesting the cyclohexyl cation is greatly influenced by the steric hindrance both on the attack to the hydroxyl group and to the phenyl ring.

The influence of the methyl groups on the ring alkylation selectivity is strictly related to the position of the substituent rather than their inductive effect. For instance, 3,5- and 2,3-dimethylphenol show, in the presence of Amberlyst 15 as a catalyst, an *ortho*–*para* ratio of 5.4 and 3.2, respectively. As a matter of fact, such a behavior suggests that the relative reactivity of the *para* positions of these compounds is about 3 times lower than the *ortho* ones. The comparison of these results with the almost equal relative reactivity of the *ortho* and *para* positions, observed in the cyclohexylation of phenol in the presence of Amberlyst 15 as a catalyst, suggests a strong effect of the steric hindrance of the methyl groups on the selectiv-



Scheme 1. Reaction paths for phenol cyclohexylation and for the cyclohexene oligomerization.

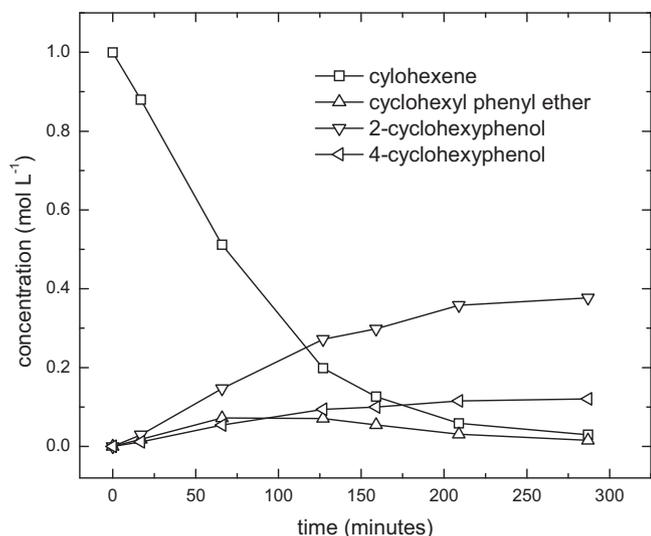


Fig. 10. Reactivity of 2,3-dimethyl phenol. Run conditions: T 358 K, solvent 1,2-dichloroethane, Amberlyst 15, 400 mg, reaction volume 10 mL.

ity. Further support to this is the equal reactivity of the *ortho* and *para* positions of the 2,5-dimethylphenol. In this case, it is likely that the methyl in 5-position has the same effect on the reactivity of the *ortho* and *para* position with the consequent equal relative reactivity.

When $\text{CH}_3\text{SO}_3\text{H}$ is used the *ortho* selectivity increases as already observed for phenol. For instance, cyclohexylation of 3,5-dimethylphenol catalyzed by $\text{CH}_3\text{SO}_3\text{H}$ shows an very high *ortho*–*para* ratio ($o/p = 140$) and in any case, for each phenol with unsubstituted *ortho* and *para* position, there is a neat increase of the *ortho* selectivity in the presence of $\text{CH}_3\text{SO}_3\text{H}$ compared to Amberlyst 15. Such a behavior is not straightforward, since it is not clear what are the reasons of such a specific *ortho* directing action of the $\text{CH}_3\text{SO}_3\text{H}$, however, either the mechanism *via* cyclohexyl phenyl ether rearrangement [37–39], or that *via* a methanesulfonic–phenol complex [40] can be responsible for this behavior.

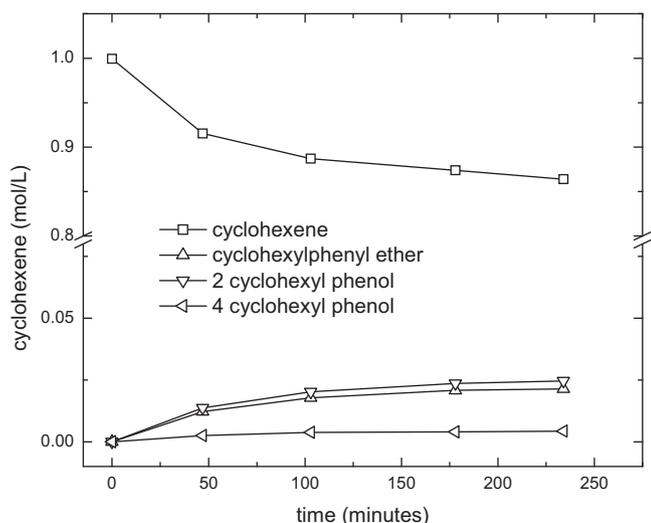


Fig. 11. Reactivity of 2,3-dimethyl phenol. Run conditions: T 358 K, solvent 1,2-dichloroethane, $\text{CH}_3\text{SO}_3\text{H}$ 180 mg, reaction volume 10 mL.

3.4. Reaction path proposed for the reactions

Alkylation, etherification and olefin oligomerization are the reactions between phenols and cyclohexene observed in the presence of acid catalysts. All the experimental evidences suggest the reaction path depicted in Scheme 1. There are three parallel and two consecutive acid catalyzed reactions. In particular, the formation of cyclohexyl phenyl ether is reversible (also the formation of the aliphatic ether is reversible [41]), while ring alkylation of phenol, cyclohexene oligomerization cyclohexyl phenyl ether rearrangement and alkylphenols isomerization are practically irreversible [39].

4. Conclusions

The reaction between phenol and cyclohexene occurs *via* a complex path, which is characterized by the formation of the cyclohexyl phenyl ether as reversible intermediate and its complete conversion to the products of ring alkylation at the end of the reaction, whenever catalyst deactivation does not occur. The reactions of *O*-alkylation, ring alkylation, ether rearrangement and cyclohexene oligomerization occur simultaneously, but the latter is practically negligible by selecting the proper solvent or carrying out the reaction in excess of phenols. In the presence of Amberlyst 15 and 36 resins the selectivity of ring alkylation of phenol seems to be driven by the typical *ortho/para* orienting effect of the hydroxyl group. On the contrary, a specific action of homogeneous systems ($\text{CH}_3\text{SO}_3\text{H}$ and AlCl_3) toward formation of the *ortho* isomers has been observed, but it is not clear what is the reason of such a behavior. The electrophilic attack of the cyclohexyl cation is strongly influenced by the steric hindrance of the methyl group as a matter of fact, the alkylation of 2,4,6-trimethylphenol practically does not occur, and the activation, due to the inductive effect to the contiguous positions of the methyl group, is negligible compared to the deactivation induced by the steric hindrance.

Acknowledgments

Financial support by Ca' Foscari University of Venice is gratefully acknowledged (Ateneo fund 2009). A thank to Dr. Davide Montin for some preliminary experiments carried out during his month in Industrial Chemistry. Finally, a special thank to Mr. Claudio Tortato for the helpful discussions.

References

- [1] K. Komiya, S. Fukuoka, M. Aminaka, K. Hasegawa, H. Hachiya, H. Okamoto, T. Watanabe, H. Yoneda, I. Fukawa, T. Dozono, in: P.T. Anastas, T.C. Williamson (Eds.), *Green Chemistry: Designing Chemistry for the Environment*, American Chemical Society, Washington, DC, 1996, p. 20.
- [2] V.C. Malshe, E.S. Sujatha, *React. Funct. Polym.* 43 (2000) 183–194.
- [3] A. Sato, I. Shimizu, E. Matsuzaka, *US* 4144279.
- [4] M.A. Harmer, Q. Sun, *Appl. Catal. A: Gen.* 221 (2001) 45–62.
- [5] W.F. Hölderich, G. Heitmann, *Catal. Today* 38 (1997) 227–233.
- [6] A. Mitsutani, *Catal. Today* 73 (2002) 57–63.
- [7] K.G. Chandra, M.M. Sharma, *Catal. Lett.* 19 (1993) 309–317.
- [8] H. Zhang, S.M. Mahajani, M.M. Sharma, T. Sridhar, *Chem. Eng. Sci.* 57 (2002) 315–322.
- [9] A. de Angelis, C. Flego, P. Ingallina, L. Montanari, M.G. Clerici, C. Carati, C. Perego, *Catal. Today* 65 (2001) 363–371.
- [10] R.A. Rajadhyaksha, D.D. Chaudhari, *Ind. Eng. Chem. Res.* 26 (1987) 1276–1280.
- [11] R.H. Rosenwald, *Alkylation in Kirk Othmer Encyclopedia of Chemical Technology*, vol. 2, Wiley, 1978, p. 50.
- [12] H.W.B. Bird, *Alkylphenols in Kirk Othmer Encyclopedia of Chemical Technology*, vol. 2, Wiley, 1978, p. 73.
- [13] G.D. Yadav, S. Ganesh, Pathre, *Ind. Eng. Chem. Res.* 46 (2007) 3119–3127.
- [14] G.D. Yadav, P. Kumar, *Appl. Catal. A: Gen.* 286 (2005) 61–70.
- [15] N. Bhatt, A. Patel, *J. Mol. Catal. A: Chem.* 264 (2007) 214–219.
- [16] R. Anand, K.U. Gore, B.S. Rao, *Catal. Lett.* 81 (2002) 33–41.
- [17] R. Amandi, K. Scovell, P. Licence, T.J. Lotz, M. Poliakov, *Green Chem.* 9 (2007) 797–801.
- [18] G.D. Yadav, G.S. Pathre, *J. Mol. Catal. A: Chem.* 243 (2007) 77–84.

- [19] M.M. Sharma, *React. Funct. Polym.* 26 (1995) 3–23.
- [20] A.J. Hoefnagel, H. van Bekkum, *Catal. Lett.* 85 (2003) 7–11.
- [21] K. Wilson, D.J. Adams, G. Rothenberg, J.H. Clark, *J. Mol. Catal. A: Chem.* 159 (2000) 309–314.
- [22] P.F. Siril, H.E. Cross, D.R. Brown, *J. Mol. Catal. A: Chem.* 279 (2008) 63–68.
- [23] A. Akelah, A. Moet, *Functionalized Polymers and Their Applications*, Chapman and Hall, 1990.
- [24] G.A. Olah, A.M. White, D.H. O'Brien, *Chem. Rev.* 70 (1970) 561–591.
- [25] G.A. Olah, G.K. Surya Prakash, J. Sommer, *Superacids*, J. Wiley, 1985, p. 90.
- [26] N.S. Isaacs, *Physical Organic Chemistry*, Longman, 1987, p. 395.
- [27] Y. Tsuji, M.M. Toteva, H.A. Garth, J.P. Richard, *J. Am. Chem. Soc.* 125 (2003) 15455–15466.
- [28] R. Klimkiewicz, H. Grabowska, H. Teterycz, *Appl. Catal. A: Gen.* 246 (2003) 125–136.
- [29] B. Chaudhuri, M.M. Sharma, *Ind. Eng. Chem. Res.* 30 (1991) 227–231.
- [30] E. Modrogan, M.H. Valkenberg, W.F. Hoelderich, *J. Catal.* 261 (2009) 177–187.
- [31] Q. Ma, D. Chakraborty, F. Faglioni, R.P. Muller, W.A. Goddard, T. Harris, C. Campbell, Y. Tang, *J. Phys. Chem. A* 110 (2006) 2246–2252.
- [32] B. Bjoerkqvist, H. Toivonen, *J. Chromatogr.* 178 (1979) 271–276.
- [33] G.W. Roberts, in: P.N. Rylander, H. Greenfield (Eds.), *Catalysis in Organic Synthesis*, Academic Press, 1976, p. 1.
- [34] S. Kajount, B.M. Kierman, D.R. Brown, H.G.M. Edwards, J.A. Dale, S. Plant, *Catal. Lett.* 85 (2003) 33–40.
- [35] N.C. Marziano, A. tommasin, C. Tortato, *J. Chem. Soc. Trans. 2* (1991) 1575–1580.
- [36] C. Reichardt, *Solvents and Solvent Effects in Organic Chemistry*, 2nd ed., VCH, Weinheim, 1988, p. 22.
- [37] K. Schofield, *Aromatic Nitration*, Cambridge University Press, Cambridge, 1980.
- [38] P.B.D. De La Mare, J.H. Ridd, *Aromatic Substitution*, Butterworths Scientific Publications, London, 1959.
- [39] C.B. Campbell, A. Onopchenko, D.C. Young, *Ind. Eng. Chem. Res.* 29 (1990) 642–647.
- [40] G. Sartori, F. Bigi, R. Maggi, A. Arienti, *J. Chem. Soc. Perkin Trans. 1* (1997) 257–260.
- [41] J.F. Izquierdo, F. Cunill, M. Vila, M. Jhorra, J. Tejero, *Ind. Eng. Chem. Res.* 33 (1994) 2830–2835.