

Applications of Dimethyl Carbonate for the Chemical Upgrading of Biosourced Platform Chemicals

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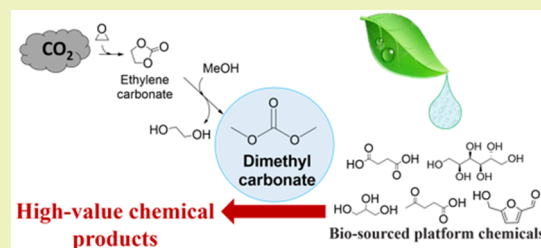
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ABSTRACT: Dimethyl carbonate (DMC) is a nontoxic compound currently prepared from CO₂ as a building block, which displays a versatile reactivity for multiple applications including, particularly, the implementation of sustainable protocols for the conversion of biosourced substrates. Among them, this paper will survey representative cases of DMC-mediated methylation and carboxymethylation reactions by which platform chemicals including glycerol and its derivatives, succinic and levulinic acids, furan-derived compounds as 5-HMF and FDCA, and sorbitol are transformed into added-value compounds. By their intrinsic nature, these processes typify genuine green archetypes combining the upgrading of renewables with the use of safe reagents, catalysis, recycle, minimal, if any, production of wastes, and solvent-less conditions.

KEYWORDS: Dimethyl carbonate, Biomass-derived platform molecules, Methylation, Carboxymethylation, Catalysis, Biorefinery



INTRODUCTION

The growing awareness of modern society for global environmental issues mostly including the finite availability of fossil resources and climate change is changing life styles moving consumers toward more responsible choices of products (plastics, materials, fuels, and even food) with reduced or neutral carbon footprint.^{1,2} In this respect, the development of biorefineries able to process biomass and further convert the biosourced substrates of the primary transformation into high-value chemical products is a highly desirable target for a sustainable management of the natural carbon cycle.³ The analysis of this scenario, however, highlights significant challenges associated on one side with the economic sustainability of biomass conversion which needs to integrate the production of chemicals to that of biofuels, and on the other side with a deficiency of technologies for the upgrading of renewables, an aspect which is further exacerbated by the large number of potentially accessible biobased compounds. Plastics are among the best models exemplifying how the choices of feedstocks and processing technologies not only affect the economics of the productive chain but also medium–long-term impact on the environment. Indeed, a new promising plastic typically requires 2–3 years for preliminary applications, 2–6 years to reach a platform position, and up to 20–40 years for market penetration in the production of materials with enhanced technical functions on a scale over 100 000 tonnes.⁴ A cogent strategy to cope with these issues and combine safety and environmental protection with economics is by tailoring syntheses in which clean reagents and solvents are used for the catalytic upgrade of

renewable platform chemicals. CO₂ and its derivatives, particularly dialkyl carbonates, can play a remarkable role in this respect. Indeed, regarding biomass originated by atmospheric carbon dioxide which is converted into chemicals with sustainable (sunlight) energy, the approach aims at squaring the carbon cycle.⁵ The model case of dimethyl carbonate (DMC), the simplest term of the dialkyl carbonates series, well illustrates the concept. Since the synthesis of DMC has been extensively reviewed even in recent times,^{6–8} evolution and details of these studies will not be further commented here except for stressing that the industrial production of DMC integrated in the Asahi–Kasei process for the manufacturing of polycarbonate, represents one of the best examples of green and sustainable transformations available on a large scale (Scheme 1).⁹

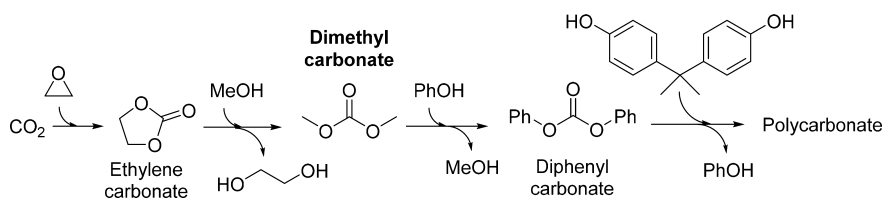
CO₂ is initially used as a safe building block for the insertion of into ethylene oxide, producing ethylene carbonate which, in turn, undergoes a transesterification reaction with methanol carried out in a continuous mode. Pure dimethylcarbonate is thus achieved. Then, in the same plant, DMC is used for a second transesterification reaction to synthesize diphenylcarbonate which is the last intermediate for the manufacture of polycarbonate. The overall sequence proceeds with high yields and selectivities in all steps; intermediate products including ethylene carbonate, DMC, MeOH, diphenylcarbonate (DPC), and PhOH are used as reactants toward the final polymer, all

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Scheme 1. Synthesis of DMC Integrated in the Polycarbonate Manufacture from Asahi–Kasei Process



77 processes are catalytic reactions with no wastes, and no water is
78 required for disposal treatments. As another remarkable
79 feature, DMC is obtained as a nontoxic reagent.

80 From the chemical standpoint, DMC behaves as an
81 ambident electrophile due to the presence of two active
82 centers, the methyl and the carbonyl carbons, in the molecule.
83 Both methylation and methoxycarbonylation reactions are
84 therefore observed with several types of O-, S-, C-, N-, and P-
85 nucleophiles including phenols and alcohols, methylene active
86 compounds, amines and phosphines.^{10–12} Conditions and the
87 nature of the catalysts help to differentiate the two reaction
88 paths: below or at the refluxing temperature (90 °C), DMC
89 acts primarily as a methoxycarbonylating agent yielding
90 carbonate interchange products (e.g., asymmetrical methyl
91 alkyl carbonates, high dialkyl carbonate homologues, and
92 carbamates), while at $T \geq 160$ °C, methylation reactions
93 preferentially occur forming methyl ethers and tioethers and
94 with high selectivity, mono-*N*-methyl amines. Of note, DMC-
95 mediated reactions are (i) catalyzed by both bases (alkaline
96 carbonates, organo-bicyclo compounds as TBD, DBU, and
97 DABCO, hydrotalcites, etc.) and protic- or Lewis-acid systems,
98 (ii) often do not require additional solvents since DMC serves
99 both as a reagent and a reaction medium, and (iii) coproducts
100 are methanol, recyclable to the synthesis of DMC, and CO₂
101 (only in the case of methylations), which do not involve
102 disposal issues.¹³

103 Overall, the nontoxicity, the favorable physicochemical
104 profile, and the versatile reactivity make DMC an ideal vector
105 of both CO₂ and methyl functions and also for the valorization
106 of biobased derivatives.

107 ■ DMC FOR THE UPGRADING OF TOP PLATFORM 108 CHEMICALS

109 In the past 15 years, massive efforts have been addressed to the
110 identification of the most promising biomass-derived com-
111 pounds. Starting from the first extensive analysis carried out in
112 2004 by U.S. Department of Energy,¹⁴ selection criteria of
113 substrates have been more and more refined over the years to
114 include and examine market attractiveness and competitive-
115 ness, technologies for high volume products, potential for
116 supply chain integration and replacement of existing
117 petrochemical derivatives, etc.^{3,15–18} However, the current
118 list of the so-called top biobased platform chemicals still
119 includes most of the originally identified compounds,
120 particularly ethanol, functionalized mono- and dicarboxylic
121 acids (lactic-, levulinic-, hydroxypropionic-, and succinic- acid),
122 furan-based products as furfural, hydroxymethylfurfural
123 (HMF), and furan dicarboxylic acid (FDCA), biohydrocarbons
124 derived from isoprene, glycerol and derivatives, and other
125 sugars such as sorbitol and xylitol. This review will examine
126 representative examples in which some of such platform
127 molecules have been upgraded by using DMC as a methylating
128 or a methoxycarbonylating agent.

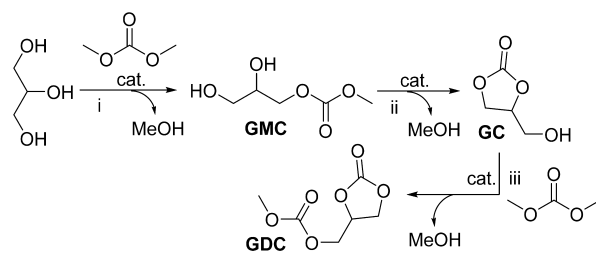
■ GLYCEROL AND DERIVATIVES

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Glycerol. DMC readily undergoes interchange carbonate
reactions (transcarbonations) with glycerol to produce either
glycerol carbonate (GC) or the corresponding glycerol
dicarbonate (GDC) (Scheme 2).¹⁹

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133 s2

Scheme 2. Transcarbonation Reactions of Dimethyl Carbonate with Glycerol



Up to three subsequent transcarbonations may occur. The
first two processes (i, ii) however, often take place almost
concurrently: the intermediate glyceryl methyl carbonate
(GMC) is not isolated due to easy cyclization reaction
which yields GC with very high selectivity and yields, both
typically >90%, at 40–80 °C in a few hours. The formation of
GDC instead requires an excess of DMC and longer reaction
times.

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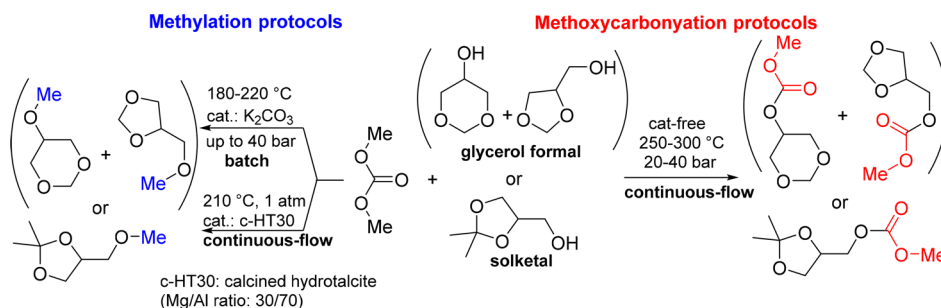
The broad spectrum of applications of GC as a low toxic
solvent in cosmetic, personal care, medicinal uses, and as an
excellent electrophilic partner for reactions of alcohols and
phenols, has fueled an enormous attention for the reaction of
Scheme 2 which certainly represents one of the most
investigated uses of DMC for the upgrading of renewable
substrates. This scenario is further witnessed by the role of GC
as a key product for sustainability in the portfolio of industrial
giants as Huntsmann and UBE.^{20,21}

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Base catalysts are by far more effective for the synthesis of
GC than acid systems, due to their ability of activating glycerol
through the formation of a glyceroxide anion which acts as a
powerful nucleophile on DMC (see Scheme 2). Starting from
seminal works proposing K₂CO₃ for the transcarbonation of
DMC with glycerol,²² several bases have been reported, mostly
as heterogeneous systems including NaOH/γ-Al₂O₃, KF
supported on Al₂O₃, SiO₂, ZnO, ZrO₂, H-beta, and carbon,
K-exchanged zeolites, and metal-doped calcined hydro-
talcites.^{23–26} The literature, however, highlights a pre-eminent
role of commercially available CaO to catalyze the reaction:
features and performance of CaO have demonstrated its
potential for the implementation of the synthesis of GC even
on an industrial scale.^{27,28} The process typically offers
quantitative (glycerol) conversion at 95 °C, with GC yield of
95%. Although the catalyst may deactivate by forming calcium
glycerate [Ca_x(OH)_y(CO₃)_z], this has a negligible
impact on the techno-economic feasibility of the synthesis

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167
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Scheme 3. Upgrading of Glycerol Acetals by DMC



169 because fresh commercial CaO is a cheap material and the
 170 disposal of the exhausted catalyst does not pose any
 171 environmental issue. Of note, CaO has been recently proposed
 172 for the synthesis of GC from DMC and crude glycerol under
 173 MW-irradiation. At 65 °C, a 91% conversion of the crude
 174 reagent (glycerol, MeOH, and NaOMe as residues of biodiesel
 175 manufacture) was achieved after only 5 min, with 85% yield of
 176 GC.²⁹

177 Biocatalysts have also been investigated for the trans-
 178 carbonation of DMC with glycerol. A major hurdle for the
 179 setup of the reaction is the poor mutual solubility of reactants
 180 which imposes either additional solvents (i.e., *t*-BuOH,
 181 acetonitrile, MTBE) or surfactants (i.e., Tween 80 and Brij)s
 182 able to avoid or minimize the preferential adsorption of
 183 hydrophilic glycerol on the enzyme surface.^{30,31} *Candida*
 184 *antarctica* (CAL) immobilized on polyacrylic resin (Novozym
 185 435) has been reported as one of the most active and selective
 186 biocatalysts. Interestingly, a protocol has described the use of
 187 this enzyme also under solventless conditions to carry out two
 188 sequential DMC-promoted transesterification reactions by
 189 which soybean oil was first converted into biodiesel and
 190 glycerol, while the latter was concurrently transformed into
 191 GC. The overall process was optimized at 60 °C yielding
 192 conversion and selectivity to GC of 92.5% and 96.4%,
 193 respectively.³² A similar approach was followed to implement
 194 also the continuous-flow synthesis of GC using lipase B from
 195 *Candida antarctica* immobilized on Accurel MP1000 (Cal-
 196 BAcc) as a catalyst.³³ At 60 °C, CalBAcc proved effective to
 197 obtain GC starting either from a solution of pure glycerol,
 198 DMC, Brij 76 as a surfactant, and *t*-BuOH as a solvent, or a
 199 mixture of DMC–soybean oil and MTBE as a cosolvent.³⁴
 200 Varying the residence time up to 176 min, quantitative
 201 conversion and selectivity were claimed, but isolated yields of
 202 GC were not indicated. In this respect, recent reviews have
 203 stressed how the availability of immobilized enzymes is
 204 currently opening a new frontier for continuous-flow
 205 applications of biocatalysis.^{35,36}

206 The application of continuous-flow technologies to perform
 207 these types of reactions could offer significant advantages as
 208 compared to batch reactor designs. Continuous-flow systems
 209 allow for higher control over reaction conditions, quick and
 210 efficient reagent mixing, shorter reaction times, and enhanced
 211 heat and mass transfer and process intensification. Due to the
 212 aforementioned advantages, continuous-flow conditions can
 213 significantly promote processes by increasing yields and/or
 214 selectivities, as compared to batch processes. These tech-
 215 nologies also improve safety and facilitate scale up for certain
 216 applications.^{37,38}

217 Thermal, catalysts-free conditions were also explored for the
 218 reaction of DMC with glycerol. It should be noted that in the

perspective of large-scale productions, the energetic demand of
 protocols requiring high temperatures is significantly alleviated
 by integrating such processes in modern biorefinery units in
 which the recovery or exchange of (waste and excess) heat is
 managed by heat-sinks as part of cogeneration plants.³⁹ In the
 batch mode, the thermal transcarbonation protocol for the
 synthesis of GC was productive at 300 °C and 20 MPa,
 yielding GC in a 98% yield after 15 min. Both the use of lower
 pressure ≤ 5 MPa or a crude reagent [mixture of glycerol water
 (10 wt %), salts (20 wt %), and soaps (35 000 ppm)]
 decreased yields to 40–60%, because the contact of reagents as
 condensed phases was less effective, and at the same time,
 alkaline impurities of crude glycerol favored the decomposition
 of GC into glycidol.^{40,41} The thermal reaction of DMC with
 glycerol was investigated also by one of us who highlighted
 how the products selectivity and yields could be tuned by
 changing the reaction conditions, specifically the reactant ratio
 and time in the batchwise mode and the pressure and the
 residence time in the continuous-flow mode:⁴² accordingly, in
 an autoclave at 180 °C (batch), either GC or glycerol
 dicarbonate (GDC) were obtained selectively in 84% and 80%
 yield, respectively; while at 230–250 °C and 50 bar (flow rate
 0.1 mL min⁻¹), the flow-reaction yielded GC as the primary
 product (83–92% yield).

Glycerol Acetals. The most studied acetals of glycerol
 (GAs) are the simplest terms of the series, namely glycerol
 formal and solketal, which are obtained by acid-catalyzed
 condensation of glycerol with formaldehyde and acetone,
 respectively. These model GAs find applications as such in the
 field of biobased and nontoxic solvents and fuel additives, but
 they also display a typically alcohol-like reactivity which allows
 their chemical upgrading into the corresponding ethers and
 esters.^{43,44} In this respect, DMC has been extensively
 investigated by our group, as both a methoxycarbonylating
 and a methylating agent of GAs in a variety of conditions
 including catalytic, thermal (cat-free), batch, and continuous-
 flow modes. Results are summarized in Scheme 3.

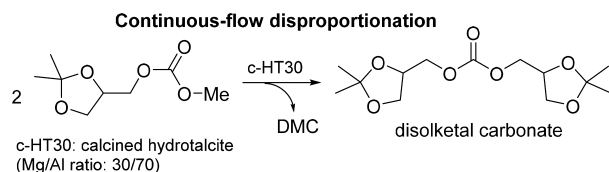
A thermal (catalyst-free) transcarbonation was effectively
 performed under continuous-flow conditions, at 275–300 °C
 and 20–40 bar.⁴⁵ GAs yielded the corresponding mono-
 transesterification products with a selectivity up to 98% at a
 substantially quantitative conversion (Scheme 3, right). The
 reaction was remarkably affected by the pressure whose effect
 was consistent with the partition of DMC from the vapor to
 the liquid phase. Accordingly, an abrupt improvement of the
 conversion (from 1–2% to ~85%) was observed at ~35 bar.

Since DMC-mediated methylation reactions display an
 activation barrier higher than methoxycarbonyl (transcarbona-
 tion) processes, the etherification of GAs required both
 temperatures as high as 180–220 °C and the compulsory

269 presence of a catalyst (Scheme 3, left). Such reaction was first
 270 reported under batch conditions in the presence of K_2CO_3 as a
 271 basic catalyst.⁴⁰ Although excellent selectivity and yields up to
 272 99% and 86–99%, respectively, were achieved toward the
 273 methyl ethers of both glycerol formal and solketal, a slow
 274 kinetics was noticed, and an extensive side-decarboxylation of
 275 DMC took place generating a high autogenous pressure. The
 276 reaction outcome was greatly improved in the continuous-flow
 277 mode by using a catalyst (c-HT30) composed of a mixture of
 278 Mg/Al oxides obtained by the calcination of a hydrotalcite
 279 precursor (Scheme 3, left, bottom).⁴⁶ Under such conditions,
 280 quantitative conversion and O-methylation selectivities were
 281 reached at atmospheric pressure, and even more importantly,
 282 the productivity of the process ($\sim 2 \text{ g}_{\text{prod}} \text{ g}_{\text{cat}}^{-1} \text{ h}^{-1}$) was up to
 283 200 times higher than that of the previous batchwise method.
 284 Moreover, the flow-mode protocol proved effective also for the
 285 etherification of glycerol carbonate and tetrahydrofurfuryl
 286 alcohol, the latter deriving from sugars dehydration.

287 To conclude this section, recently, a continuous-flow
 288 procedure was implemented to further convert asymmetrical
 289 methyl alkyl carbonates obtained from GAs and DMC, into the
 290 corresponding symmetrical dialkyl carbonates.⁴⁷ Scheme 4
 291 illustrates the model case of the solketal derivative.

Scheme 4. Catalytic Disproportionation of Solketal Methyl Carbonate



292 At 210 °C and atmospheric pressure, in the presence of the
 293 same catalyst above-mentioned (c-HT30), a disproportiona-
 294 tion reaction took place yielding disolketal carbonate with
 295 selectivity and productivity up to 92% and $152 \text{ mg}_{\text{prod}} \text{ g}_{\text{cat}}^{-1}$
 296 h^{-1} , respectively (residence time: 2.5 min). The procedure
 297 proved robust and suitable to several biobased methyl alkyl
 298 carbonates, thereby further confirming the effective role of the
 299 chemistry promoted by DMC in this area.

300 ■ BIOBASED CARBOXYLIC ACIDS

301 **Succinic Acid.** Microbial-based productions of renewable
 302 succinic acid afford the corresponding salt, often as a disodium
 303 species, which must be neutralized and further converted into
 304 other derivatives, especially esters, before any use.⁴⁸ With the
 305 aim of avoiding these upstream operations that consume a

stoichiometric acid and produce waste salt, an original
 approach was proposed by integrating recovery and chemical
 upgrading of succinate using DMC as an alkylating agent.⁴⁹
 The concept is illustrated in Scheme 5.

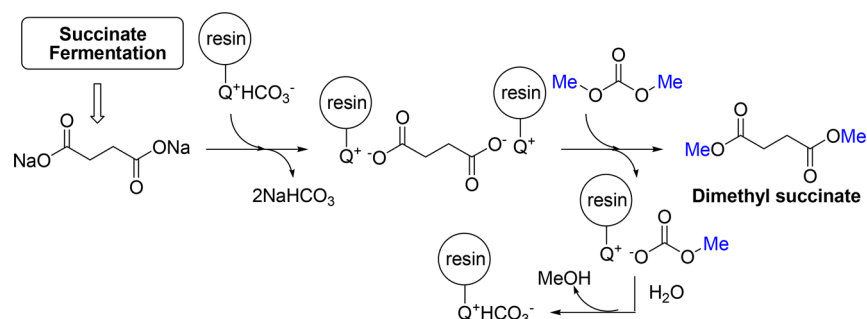
First, succinate disodium salt is captured from an aqueous
 fermentation broth by an anion exchange resin in a
 (bi)carbonate form releasing the respective (bi)carbonate
 salt. Then, at 100–120 °C, sorbed succinate undergoes an O-
 methylation reaction mediated by DMC and catalyzed by
 quaternary ammonium groups (Q^+) of the resin. This
 exemplifies a low-temperature alkylation pathway, unusual for
 DMC, which according to further study of the same group is
 affected by the nature and hydrophobicity of ammonium
 cations.⁵⁰ In the presence of water, the resulting methoxycar-
 bonate anions exchanged on to resin, decompose thereby
 restoring the original bicarbonate-based resin and releasing
 methanol. It should be noted that here few other studies are
 available for the O-methylation of carboxylic acids by DMC: in
 those cases, either superbases as DBU or combined systems as
 K_2CO_3 /tetrabutylammonium chloride and K_2CO_3 /DMSO
 were used as catalysts.^{51–53}

Levulinic Acid. Levulinic acid (LA) comes from
 saccharides through an acid-catalyzed sequence yielding at
 first 5-(hydroxymethyl)furfural (HMF) which, in turn, yields
 an equimolar mixture of LA and formic acid.⁵⁴ Among
 biobased carboxylic acids, LA has probably the highest
 potential for the market including personal care products,
 lubricants, adsorbents, electronics, photography, batteries, and
 drug delivery systems. Moreover, due to the progressive drop
 of its price from 8.8 to 13.2 \$/kg in 2000 to 5–8 \$/kg in 2015,
 a steady growth of applications and uses of LA is expected in
 the near-future.⁵⁵

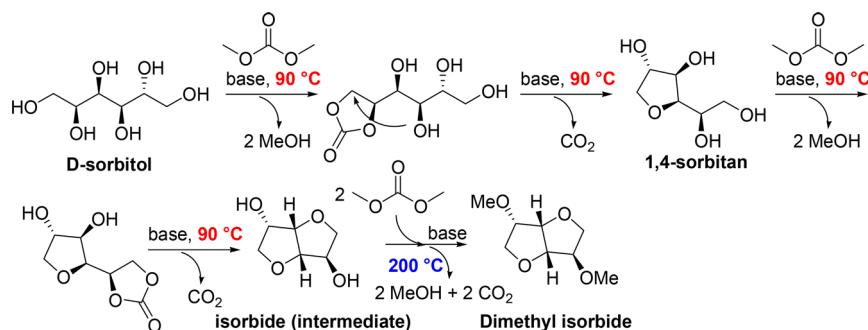
The reactivity of levulinic acid with DMC has been
 extensively investigated by our group. In the presence of
 basic catalysts, multiple products including methyl levulinate,
 dimethyl succinate, and methyl 4,4-dimethoxypentanoate (i.e.,
 dimethyl ketal of methyl levulinate) were achieved.⁵⁶ However,
 tuning of reaction conditions, mostly by changing temperature
 and cosolvents, allowed to a certain degree a control of the
 products distribution. This is shown in Scheme 6.

At 160 °C, the K_2CO_3 -catalyzed reaction of LA with DMC
 produced selectively methyl levulinate (ML, eq a), while
 increasing temperature (up to 200 °C) and adding MeOH
 prompted the unique formation of the dimethyl ketal of ML
 (eq b). Finally, moving to stronger bases as DBU, induced the
 formation of dimethyl succinate (DS) which was isolated in a
 $\sim 30\%$ yield (eq c). Mechanistic hypotheses for such reactions
 are formulated in Scheme 7.

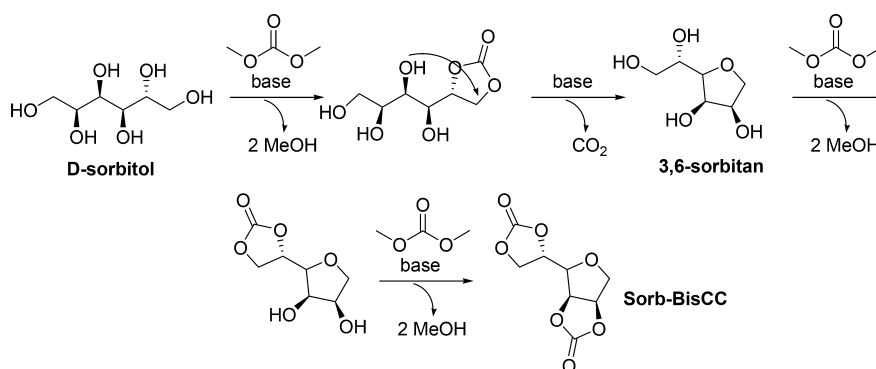
Scheme 5. Recovery of Dimethyl Succinate from Fermentative Broths, via Methylation with DMC



Scheme 9. One-Pot Two-Step Sequence for the Synthesis of Dimethyl Isosorbide from Sorbitol and DMC



Scheme 10. Formation of Sorb-BisCC from D-Sorbitol and DMC



424 S).⁶⁵ In this case, disodium 2,5-furandicarboxylate
 425 (Na_2FDCA_2) was produced by whole cell biotransformation
 426 of 5-(hydroxymethyl)furfural (HMF) by a recombinant
 427 *Pseudomonas putida*. The salt was exchanged on a macroporous
 428 Dowex resin, with a capacity up to 0.30 g FDCA_2^- per g dry
 429 resin, and finally, methylation was performed in an autoclave at
 430 100 °C with excess DMC (30 g DMC/g loaded resin). The
 431 reaction yielded 0.77 mol FDME per mol of FDCA. Authors
 432 claimed the need for a high reaction temperature to favor the
 433 alkylation kinetics, but a hurdle for this improvement was the
 434 thermal stability of the resin.

435 **Sorbitol.** The major interest for D-sorbitol as a biobased
 436 platform chemical is mostly due to its conversion to isosorbide
 437 (1,4:3,6-dianhydro-D-glucitol), an anhydro cyclic derivative
 438 which finds applications and potential uses as a building block
 439 for new polymers and functional materials, new organic
 440 solvents, intermediate for medicinal and pharmaceutical
 441 sectors, and even for fuels or fuel additives.^{66,67} Among
 442 different methods for the synthesis of isosorbide, an appealing
 443 protocol has been conceived through the straightforward
 444 reaction of D-sorbitol and DMC in the presence of base
 445 catalysts (K_2CO_3 , MeONa, DBU).^{68–70} The overall cyclization
 446 process proceeds via two sequential DMC-mediated reactions,
 447 specifically a methoxycarbonylation followed by an intra-
 448 molecular alkylation, in which DMC acts both as a leaving
 449 group and a sacrificial molecule. In an extension of this study, a
 450 procedure was implemented to perform in one-pot both the
 451 preparation of isosorbide and its further upgrading to the
 452 corresponding dimethyl derivative, a green industrial solvent of
 453 interest also for pharmaceutical additives and products for
 454 personal-care (Scheme 9).

455 The reaction required a careful control of temperature, by
 456 first heating reactants mixture at 90 °C to allow the
 457 quantitative cyclization of D-sorbitol to the isosorbide

intermediate, and then at 200 °C for the second methylation 458
 step affording dimethylisosorbide. In the presence of 1,5,7- 459
 triazabicyclo[4.4.0]dec-5-ene (TBD) as a catalyst, the product 460
 was isolated in a 69% yield which is relevant if one considers to 461
 the scant reactivity of secondary hydroxyl groups of isosorbide. 462
 Authors proposed that the molecule backbone of isosorbide, 463
 particularly its rigid V-shaped configuration, allowed the 464
 formation of strong intramolecular H-bonds affecting the 465
 reactivity. 466

Another interesting product coming from the base-catalyzed 467
 reaction of sorbitol and DMC is the bis-cyclocarbonate 468
 derivative, Sorb-BisCC (1R,4S,5R,6R)-6-(1,3-dioxolan-2-one- 469
 4-yl)-2,4,7-trioxo-3-oxy-bicyclo[3.3.0]octane), that is a useful 470
 building block for short and long polyols, or novel biobased 471
 nonisocyanate polyurethanes (NIPU)^{65,71,72} (Scheme 10). 472 s10

In this case, a transcarbonation of DMC starting from a 473
 primary hydroxyl group at position 6 forms a cyclic carbonate 474
 intermediate which, upon nucleophilic attack by a secondary 475
 hydroxyl and subsequent decarboxylation, yields 3,6-sorbitan. 476
 Two further transcarbonation reactions of additional DMC 477
 and residual hydroxyl functions give Sorb-BisCC as a final 478
 product in a 40% yield. The reaction outcome was controlled 479
 by temperature and solvation effects; specifically, the onset of 480
 competitive formation of isosorbide (Scheme 9) was observed 481
 above 80 °C and favored by cosolvents (e.g., dioxane and 482
 MeOH). 483

CONCLUSIONS 484

This paper has reviewed recent advances on the use of DMC as 485
 a transcarbonation and a methylation reagent for the upgrading 486
 of biosourced platform chemicals focusing the discussion of 487
 synthetic strategies on the choice of catalysts and reaction 488
 conditions including both continuous-flow and thermal 489
 (noncatalytic) processes. Dimethyl carbonate often offers one 490

of the best options to meet not only criteria of safety but also to intensify the process by improving productivity, minimizing the use of solvents, and optimizing downstream operations (recycle, separation, and purification methods). It should be noted that coproducts of DCM-mediated transformations are MeOH and CO₂ (the latter only for methylation reactions), which can be directly or indirectly recycled for the synthesis of DMC itself or easily conveyed to other uses. Although costs of DMC and energy demand for its reactions may still not be competitive with respect to processes carried out by conventional (and highly dangerous/toxic) carboxylating and methylating agents as phosgene, methyl halides, and dimethylsulfate), a concrete perspective to alleviate this issue can be devised by integrating synthesis and use of DMC in a biorefinery plant with modern technologies for recovery/recycle of waste heat and reagents/solvent.

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Notes

The authors declare no competing financial interest.

Biographies



Maurizio Selva is a full professor of Organic Chemistry at the Department of Molecular Sciences and Nanosystems, University Ca' Foscari Venezia (Italy). Since the beginning of his academic career in the early 90s, his main research interests focused on the implementation of eco-friendly organic syntheses based on clean reagents, catalysts, and solvents. More specifically, the development of green catalytic techniques for the upgrading of bio-based platform chemicals using dense CO₂ and dialkyl carbonates and multiphase systems assisted by ionic liquids are among the current topics of research of Prof. Selva.



Alvise Perosa earned his Ph.D. in Chemistry from Case Western Reserve University in 1996 and is currently associate professor of Organic Chemistry at Ca' Foscari University Venice. He was Fulbright Fellow at Case Western Reserve University, Endeavour Research Fellow at the University of Sydney and is currently a Fellow of the Royal Society of Chemistry. Alvise sits on the Editorial Advisory Boards of Green Chemistry (RSC) and ACS Sustainable Chemistry and Engineering (ACS). Alvise's interests include research, teaching, and outreach in green chemistry with specific focus on chemicals from renewable resources, green chemicals from carbon dioxide, ionic liquids, catalysis, supercritical fluids, and multiphase reaction systems.



Daily Rodríguez-Padrón is a Ph.D. student at the Universidad de Córdoba (Group FQM-383). She received her Degree in Chemistry at the University of Havana, Cuba in 2013, and her Master's Degree at the University of Córdoba, Spain in 2016. After finishing her undergraduate studies, she worked at the Center of Genetic Engineering and Biotechnology, in Cuba, for one year, especially on synthesis of peptides. As part of her Ph.D. investigations in the Group FQM-383 "Nanochemistry and biomass Valorization" she has worked on the design of nanomaterials through mechanochemical grinding processes, the functionalization of nanoparticles with proteins, and their applications in catalysis, green chemistry, biomass valorization, and electrochemistry with a strong sustainable character looking forward to ameliorate climate change.



553 Rafael Luque is full professor from Departamento de Química
554 Organica at Universidad de Cordoba (Spain), where he graduated in
555 2005, after spending a postdoctoral stay at The Green Chemistry
556 Center of Excellence from the University of York. With various
557 positions held in China (Chinese Academy of Sciences, Xiamen
558 University), Brazil (Universidade Federal de Pelotas), France
559 (Sorbonne Universites UTC), and Russia (RUDN University) as
560 visiting/distinguished professor, Rafael, 2018 Highly Cited Research-
561 er, belongs to group FQM-383 which has extensive expertise in
562 nanoscale chemistry, heterogeneous catalysis, green chemistry, and
563 biomass and waste valorization.

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